

# Performance Analysis of Efficient Heat Flow by Compact types Heat Exchanger

<sup>1</sup>Vishal Srivastava, <sup>2</sup>Dr.Sohail Bux

<sup>1</sup>M. Tech Scholar, <sup>2</sup>Professor

<sup>1</sup>Department of Mechanical Engineering, Agnos College of Technology Bhopal, (M.P.)

<sup>2</sup>Department of Mechanical Engineering, Agnos College of Technology Bhopal, (M.P.)

Email:- [vishal1912@gmail.com](mailto:vishal1912@gmail.com), [buxsohail@gmail.com](mailto:buxsohail@gmail.com)

**Abstract-** Compact heat exchangers are one of the most critical components of many cryogenic components; they are characterized by a excessive heat transfer surface area per unit volume of the exchanger. The heat exchangers having surface area density ( $\beta$ ) greater than seven hundred  $m^2/m^3$  in either one or more sides of two-stream or multi stream heat exchanger is called as a compact heat exchanger. Platefin heat exchanger is a type of compact heat exchanger which is widely used in automobiles, cryogenics, space applications and chemical industries. The platefin heat exchangers are mostly used for the nitrogen liquefiers, so they need to be highly efficient because no liquid nitrogen is produced, if the effectiveness of heat exchanger is less than 87%. So it becomes necessary to test the effectiveness of these heat exchangers before setting them in cooperation

**Keywords:** Performance Analysis, Heat glide, Heat exchanger

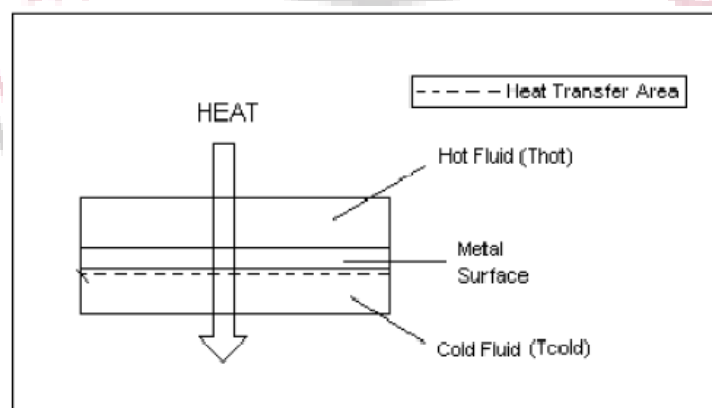
## 1. Introduction

A heat exchanger is a device to transfer heat from a hot fluid to cold fluid across an impermeable wall. Fundamental of heat exchanger principle is to facilitate an efficient heat flow from hot fluid to cold fluid. This heat flow is a direct function of the temperature difference between the two fluids, the area where heat is transferred, and the conductive/convective properties of the fluid and the way with the flow state. This relation was formulated through Newton and referred to as Newton's law of cooling, that is given in Equation (1)

$$Q = h \cdot A \cdot \Delta T \quad (1) \dots\dots\dots (1)$$

Where  $h$  is the heat transfer coefficient [ $W/m^2K$ ], where fluid's conductive/convective properties and the flow state comes in the picture,  $A$  is the heat transfer area [ $m^2$ ], and  $T$  is the temperature difference [ $K$ ]. Figure.1 shows the basic heat transfer mechanism.[1]

Heat exchangers are one of the vital components in diverse engineering plants and systems. So the design and construction of heat exchangers is often vital for the proper functioning of such systems. It has been shown in that the low temperature plant life based on Lind



**Fig. 1 Basic heat transfer mechanism**

Hampson cycle cease to produce liquid if the effectiveness of the heat exchanger is below 86.9%. On the other hand in aircrafts and automobiles, for a given heat obligation, the volume and weight of the heat exchangers should be as minimal as possible.[2]

So the main requirement for any heat exchanger is that it should be able to transfer the required amount of heat with a very high effectiveness. In order to increase the heat transfer in a basic heat exchanger mechanism shown below in Figure 1, assuming that the heat transfer coefficient cannot be changed, then either the temperature differences have to be increased. Usually, the best solution is that the heat transfer surface area is extended although increasing the temperature difference is logical, too. In reality, it may not be so meaningful to increase the temperature difference because either a hotter fluid should be supplied to the heat exchanger or the heat should be transferred to a colder fluid where neither of them are usually available. For both cases either to supply the hot fluid at high temperature or cold fluid at lower temperature extra work has to be done. Furthermore increasing the temperature difference more than enough will cause unwanted thermal stresses on the metal surfaces between two fluids. This usually results in the deformation and also decreases the life span of those materials. As a result of these facts, increasing the heat transfer surface area generally is the best engineering approach.[3]

The above requirements have been the motivation for the development of a separate class of heat exchangers known as Compact heat exchangers. These heat exchangers have a very excessive heat transfer surface area with respect to their volume and are associated with high heat transfer coefficients. Typically, the heat exchanger is called compact if the surface area density ( $\beta$ ) i.e. Heat transfer surface area per unit volume is greater than seven-hundred  $m^2/m^3$  in either one or more sides of two-stream or multi stream heat exchanger. The compact heat exchangers are lightweight and also have a lot smaller footprint, so they are exceptionally desirable in many applications.[4]

## 2. Literature review

Recovering the thermal power contained in waste warmth that is expelled from an interplay at a temperature sufficiently higher than the ambient temperature may be done profitably for some of programs. Various experiments have been performed within the place to check various techniques of electricity regulation and framework improvement.

Heat Exchangers, a bit of hardware designed for efficient hotness transfer from one medium to any other, had been studied with the aid of [5]. A stable wall may separate the media a good way to save you any mixing or any interplay among them. Heat exchangers are broadly used in industries such space heating and cooling, strength technology, synthetic chemistry, petro chemistry, oil refining, and sewage remedy. An automobile radiator is a not unusual instance of a warmth exchanger, since it transfers warmth from the engine's hot cooling liquid, water, to the air passing via the radiator. It is normally agreed that the plate warmth exchanger is the maximum realistic and cost-effective technique of moving heat between fluids. Its low rate, versatility, little protection, and brilliant warmth performance make it the quality warmth exchanger to be had.

The efficiency of a fireplace tube kettle with a very good front and screw conveyance for handling gas changed into investigated by means of [6]. Pipe gasoline heat for gas drying, preheated air for burning, and adjusting the degree of air for gas ignition prior to coming into the ignition chamber the use of the fluffy logical manipulate calculation had been crucial to the efficiency advantage. The results of the exams confirmed that heater productivity went raised through zero.41% and fuel moisture content went down by means of three% wt whilst warmth restoration and gas drying were used. When air is preheated via 35 ranges Celsius, evaporator performance will increase via 0.72 percent. With a mean air-control accuracy of 89.15%, the kettle's competency expanded by way of four.34%. When all 3 structures are put to use concurrently, a five.15 percentage boom in kettle performance, or a every year financial savings of 246.88 heaps of gasoline, is viable.

Consequently, they directed a contextual inquiry to enhance the performance of a fireplace tube heater the usage of rigid fuel on this observe's kettle.[7]

It appeared on approaches to apply renewable strength and advanced the performance of thermodynamic cycles. The growing public focus of energy and environmental worries has inspired a growing range of analysts to pursue careers in this region. Utilizing waste heat from renewable energy assets like biomass, geothermal, and sun with the usage of the natural Rankine cycle (ORC) is a sensible invention. In addition, the (waste) heat from other cycles may be protected into those as well. There has been a large uptick within the quantity of studies examining the capacity of herbal Rankine cycle (ORC) enhancements for secondary heat valorization. Power era was carried out by way of skillfully coordinating a small-scale ORC with a internet capability of 3 kW with a concentrated solar energy technology. The considerable heat supply from Photovoltaic (PV) authority turned into used via a supercritical hotness exchanger the use of R-404A as the operating medium, with a maximum temperature of a hundred C. A higher warm match within the warmth exchanger and increased common cycle productivity are both consequences of making sure supercritical hot-water glide. Using the written connections For warmth transfer, a helical loop heat exchanger became designed.[8]

### 3. Detailed Description of numerous Equipment's and Instruments used

Air is used as theas working fluid on this experiment. Theapparatus was connected toa compressor system that is capableof continuously delivering dry air .The compressed air from the compressor enters the laboratory through a control valve which is used toregulate theflow rate through the heat exchanger and then routed to the testing heat exchanger.



Fig.2 Photograph of the Experimental Setup

Table experimentally observed data.

Flow Rate (litr/min)	P1 (Kg/cm <sup>2</sup> )	P2 (Kg/cm <sup>2</sup> )	Δ c (mm of Hg)	Δ h (mm of Hg)	T1 (C)	T2 (C)	T3 (C)	T4 (C)
300	0.08	0.06	9	6	42.24	87.34	96.2	47.15
400	0.14	0.12	15	12	38.35	87.02	95.12	43.01
500	0.2	0.17	25	22	38.93	88.49	96.12	43.11
550	0.24	0.20	30	26	39.82	88..83	96.66	43.48

588	0.28	0.24	31	27	40.41	88.45	96.20	43.99
650	0.32	0.26	40	35	41.16	87.86	95.95	44.17
300	0.08	0.06	8	6	40.92	62.06	66.48	43.06
400	0.135	0.10	16	14	42.77	62.90	66.43	44.56
500	0.2	0.16	24	22	39.57	62.52	66.02	41.69
600	0.28	0.23	31	30	39.94	62.44	65.98	41.73
650	0.34	0.28	37	34	42.72	62.77	66.34	44.06

### 3. Result and Discussion

Figure three and four shows the variation of effectiveness obtained experimentally as well as with theoretical correlations and that obtained with simulation software Aspen with mass flow rate. It is seen that in both the cases effectiveness increases with mass flow rate. Experimental

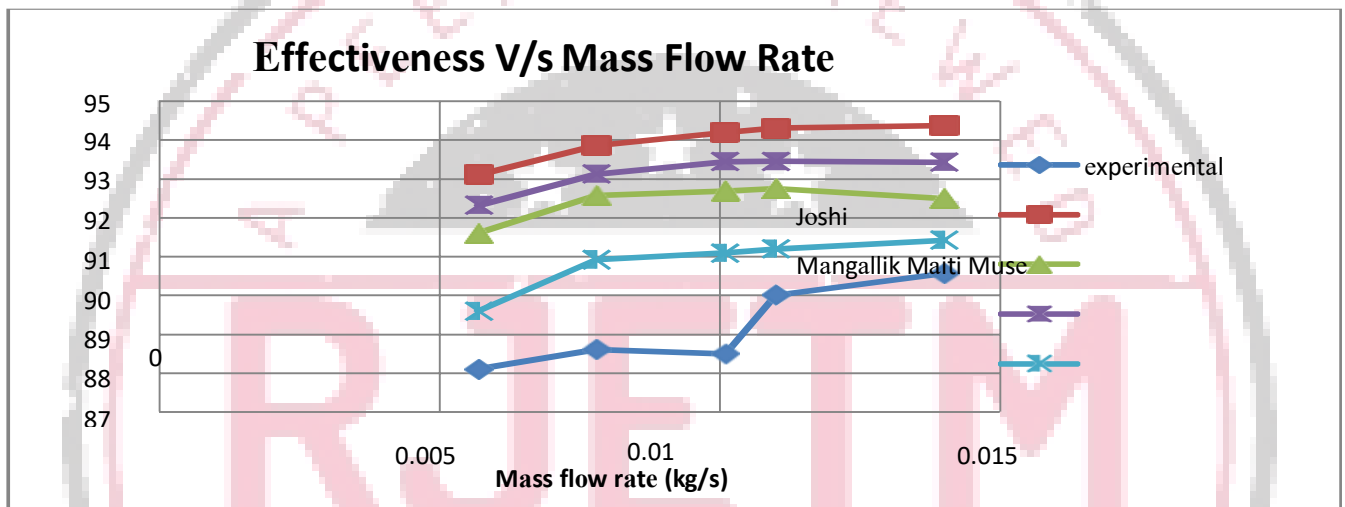


Fig. 3 Variation of effectiveness with mass flow rate (hot inlet temperature)

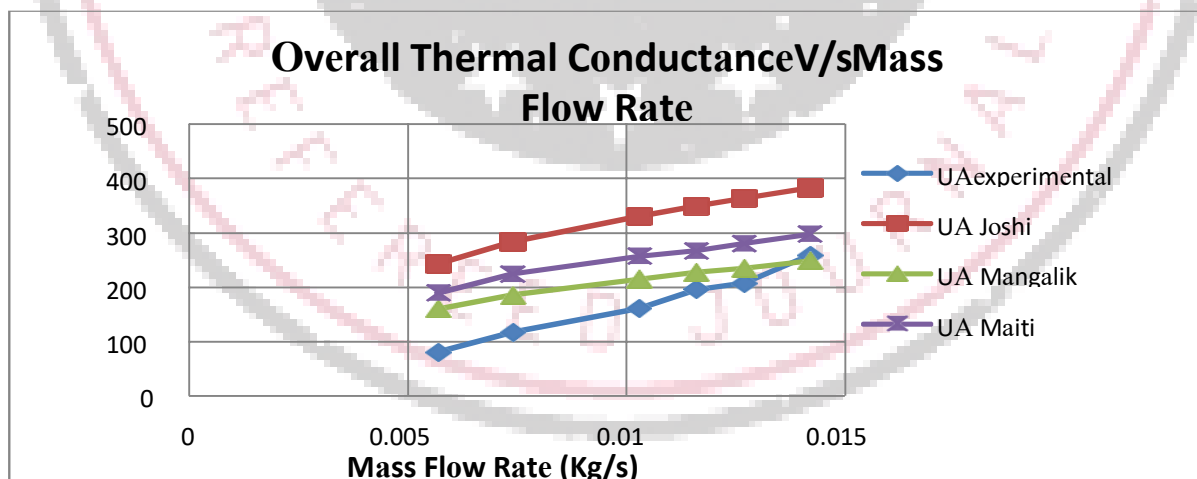


Fig. 4. Variation of overall thermal conductance with mass flow rate

### 4. Conclusions

The hot test is conducted to determine the thermal performance parameters of the available platefin heat exchanger at different mass flow rates and two different hot inlet temperatures of ninety six and 66C. An average effectiveness of ninety one% is obtained. It is found in both the cases that the effectiveness and overall thermal conductance increases with increasing mass flow rate. It is

also found that hot fluid effectiveness increases with flow rate of the fluid and agrees within 4% with the effectiveness value calculated by way of different correlations and that obtained by the usage of the simulation software, Aspen. Also the pressure drop increases with increasing mass flow rate and experimental values are more as compared to theoretical results because the losses in pipes and manufacturing irregularities have not been taken into account.

For a particular hot inlet temperature there is an optimum mass flow rate at which the difference between the hot and cold effectiveness of the heat exchanger is minimum and at this point the imbalance is also minimum. We found that the insulation which is provided in the heat exchanger has a significant effect on its performance. It is expected that the imbalance i.e. Difference between the hot and cold end temperature can be brought to a minimum level if a perfect insulation like vacuum is provided.

## Reference

1. Shivdas S. Kharche, Hemant S. Farkade "Warmth Transfer Analysis through Fin Array by Using Natural Convection", International Journal of Emerging Technology and Advanced Engineering Website: [www.ijetae.com](http://www.ijetae.com) (ISSN 2250-2459, Volume 2, Issue 4, April 2012).
2. U. S. Gawai, Mathew V. K., Murtuza S. D., "Test Investigation of Heat Transfer by Pin Fin", International Journal of Engineering and Innovative Technology (IJEIT), Vol-2, Issue 7, January 2013.
3. K. Kumar, P. Vinay, R. Siddhardha, "Warm and Structural Analysis of Tree Shaped Fin Array", Int. Diary of Engineering Research and Applications", Vol-3, Issue-6, Dec 2013.
4. V. Kumar, Dr. V. N. Bartaria, "CFD Analysis of an Elliptical Pin Fin Heat Sink Using Ansys Fluent V12.1", International Journal of Modern Engineering Research (IJMER), Vol-3, Issue 2, April 2013.
5. R. Patil, H. M. Dange, "Exploratory and Computational Fluid Dynamics Heat Transfer Analysis on Elliptical Fin by Forced Convection", International Journal of Engineering Research and Technology (IJERT), Vol-2, Issue-8, August 2013.
6. R. Patil, H. M. Dange, "Exploratory and Computational Fluid Dynamics Heat Transfer Analysis on Elliptical Fin by Forced Convection", International Journal of Engineering Research and Technology (IJERT), Vol-2, Issue-8, August 2013.
7. Amol Dhumme, H. Farkade, Heat Transfer Analysis Of Cylindrical Perforated Fins In Staggered Arrangement, International Journal Of Innovative Technology And Exploring Engineering (IJITEE), Vol-2, Issue-5, April 2013.
8. P. Singh, H. Lal, B. S. Ubhi, "Structure and Analysis for Heat Transfer Through Fin with Extensions", International Journal of Innovative Research in Science, Engineering and Technology, Vol.3, Issue 5, May 2014.
9. A. A. Walunj, D. D. Palande, "Test Analysis Of Inclined Narrow Plate-Fins Heat Sink Under Natural Convection", IPASJ International Journal Of Mechanical Engineering (IJME), Vol. 2, Issue-6, June 2014.
10. M. Reddy, G. S. Shivanshankar, "Numerical Simulation of Forced Convection Heat Transfer Enhancement by Porous Pin Fins In Rectangular Channels", International Journal of Mechanical Engineering and Technology (IJMET), Vol-5, Issue-7, July 2014.
11. M. Ehteshum, M. Ali, M. Tabassum, "Warm and Hydraulic Performance Analysis of Rectangular Fin Arrays With Perforation Size and Number". Sixth BSE International Conference on Thermal Engineering (ICTE 2014), Procedia Engineering.
12. K. Dhanawade, V. Sunnapwar, "Warm Analysis of Square and Circular Perforated Fin Arrays by Forced Convection", International Journal of Current Engineering and Technology, Special Issue-2, February 2014.
13. K. Chaitanya, G. V. Rao, "Transient Thermal Analysis Of Drop Shaped Pin Fin Array By Using CFD", International Journal Of Mechanical Engineering and Computer Applications, Vol-2, Issue 6, Dec 2014.
14. Md. Abdul Reheem Junaidi, R. Rao, S. Sadaq, M. Ansari, Thermal Analysis of Splayed Pin Fin Heat Sink, International Journal Of Modern Communication Technology and Research (IJMCTR), Vol-4, Issue-4, April 2014.

15. Sachin R. Pawar, R. Yadav, "Computational Analysis of Heat Transfer by Natural Convection from Triangular Notched Fin Array", IJST-International Journal of Science Technology and Engineering, Vol-1, Issue 10, April 2015.



